

VALORIZATION OF BIOMASS INTO HYDROGEN OR SYNGAS BY A THERMAL PROCESS

Speakers :



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Dr. MSc. Mira ABOU RJEILY

Outline



The Institute

Team 1: Energy and Heat Transfer Physics

Physics of energy transfer

Design, characterization of renewable resources valorization processes

18 Researchers

Team 2: Materials and Innovative Processes

Co-produits → Formulation/fonctionnalisation de semi-produits → Optimisation procédés → Produits

18 Researchers

iTheMIM
Institut de Thermique. Mécanique. Matériaux
53 Researchers

Team 3: Mechanics applied to Civil Engineering

17 Researchers

MATERIAUX

Béton ordinaire
Béton de fibres
Béton de chanvre

STRUCTURES

Matériau recyclé

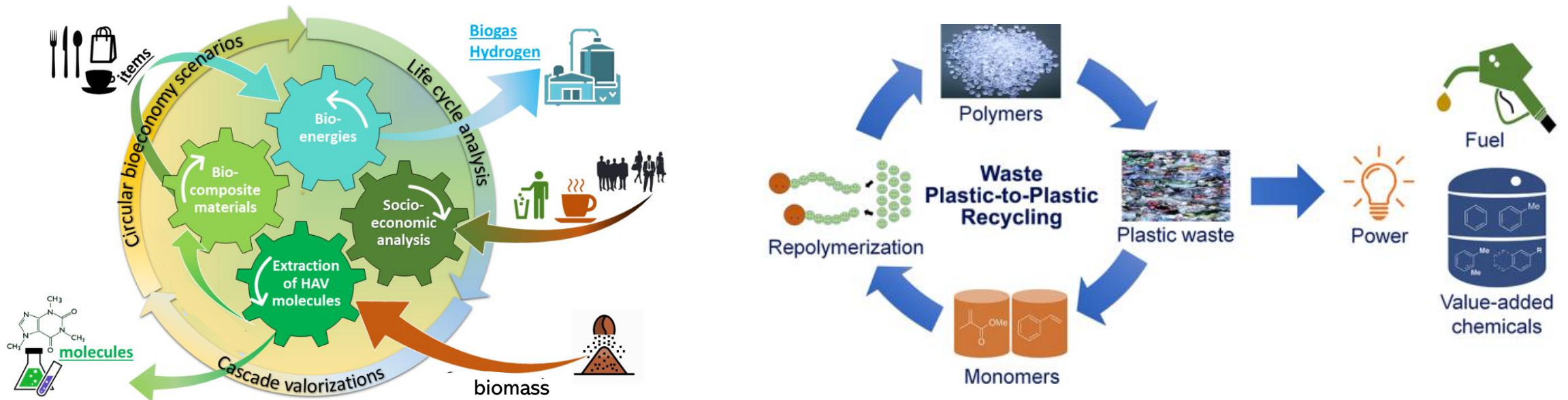
The Institute

Team 1: Energy and Heat Transfer Physics

Overall objective of Team 1 > axis #3:

Valorization of Renewable resources (biomass, sun, waste ...) for Energy purposes

- Develop efficient approaches
- (Bio sourced) wastes reaching the end of *circular economy cycle*
- High added value energy vectors (syngas, hydrogen...)



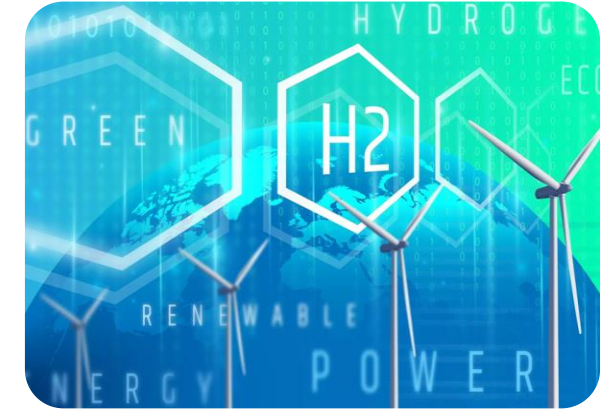
Introduction



Pollution
Growing carbon
emission
Fossil fuel depletion
Global warming
Climate change



Alternative
renewable
sustainable
energy
(solar, wind, hydro,
tidal, geothermal
biomass...)



Provide the global
energy demand for
electricity, fuels and
H₂ (transportation
and power
generation)

Introduction

Present and future hydrogen applications



Industry feedstock

- **Petroleum refinery (38.2 MT):** water treatment, hydrocracking
- **Ammonia production (31.5 MT)**



Power and heat generation

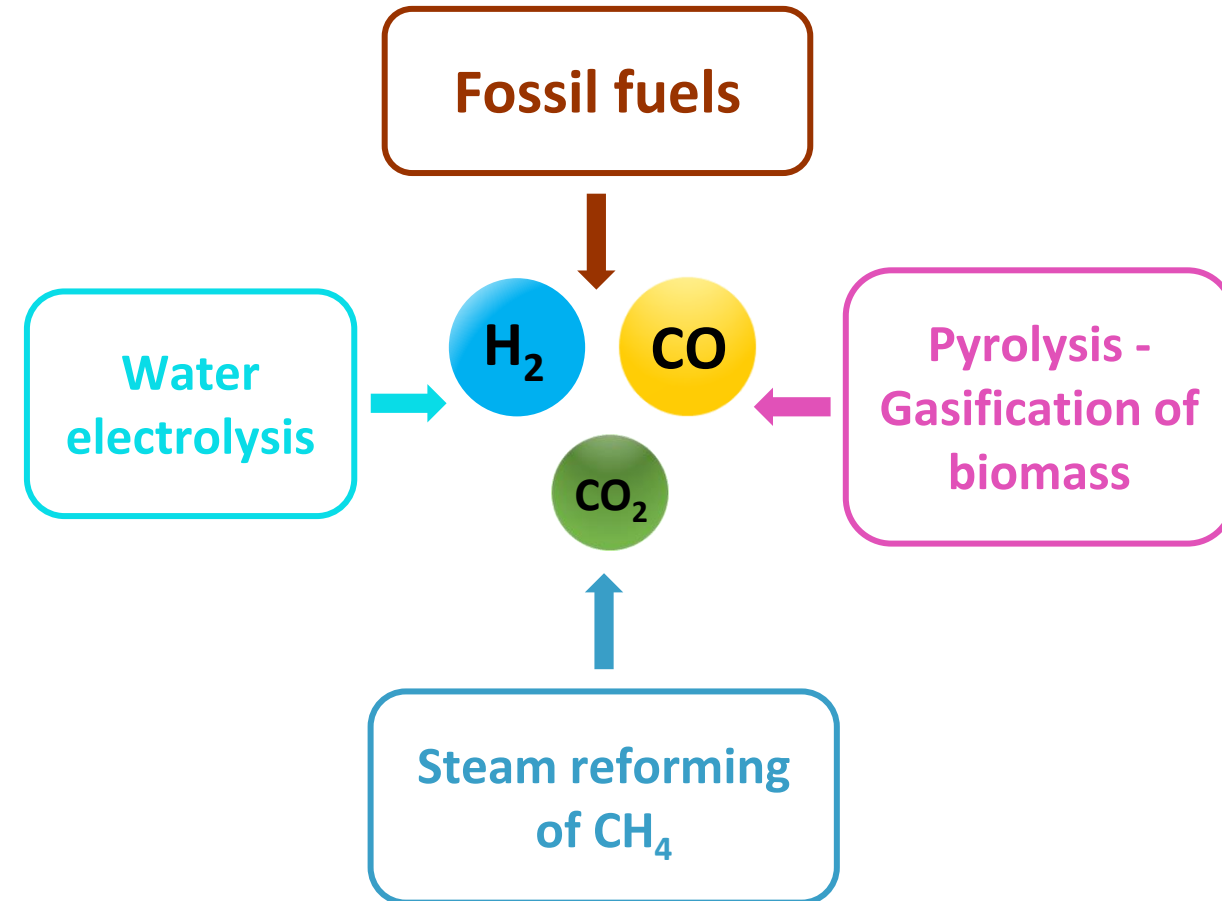
- Power generation for grid
- Heat/power for building and industry
- H₂ addition to natural gas



Transportation

- H₂ powered vehicles, trains, aircraft, shipping
- Fuel cell forklifts

Overview of syngas production



Improve the production of syngas (H_2) while reducing CO_2 and CH_4 (greenhouse gases) by valorizing the biomass (pyrolysis/catalytic reforming)

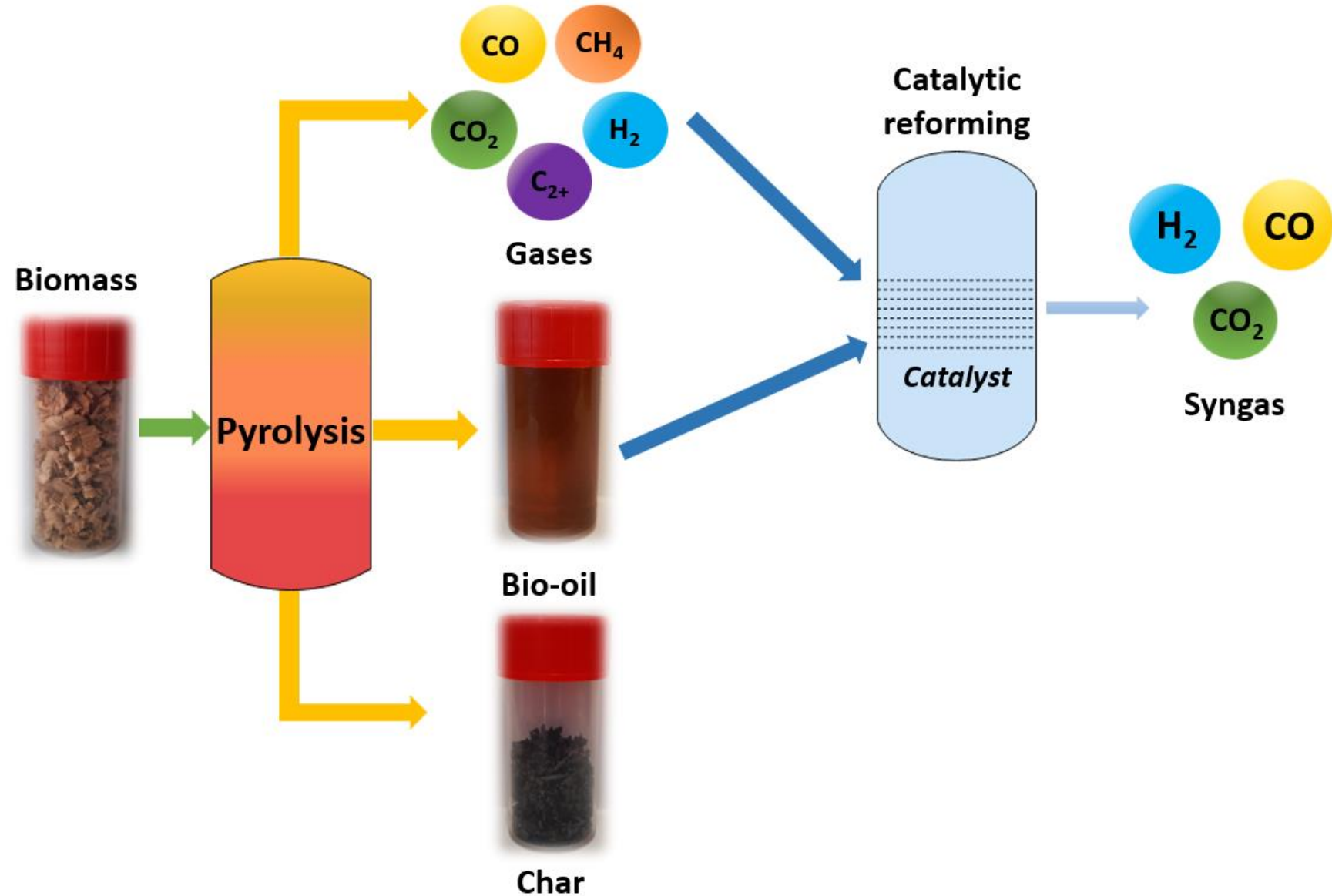
Parameters:

- Catalyst active phase
- Temperature
- External steam feed

Products:

- Gas, bio-oil, char
- Conversion rates
- Syngas production

Introduction



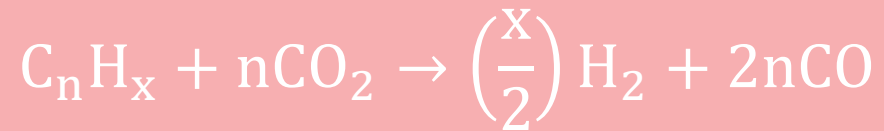
Introduction

Dry reforming (CO₂)

- Methane:



- Bio-oil:

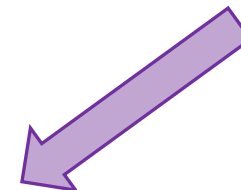
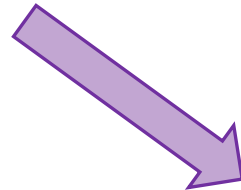
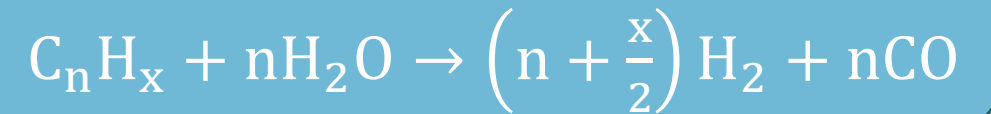


Steam reforming (H₂O)

- Methane:

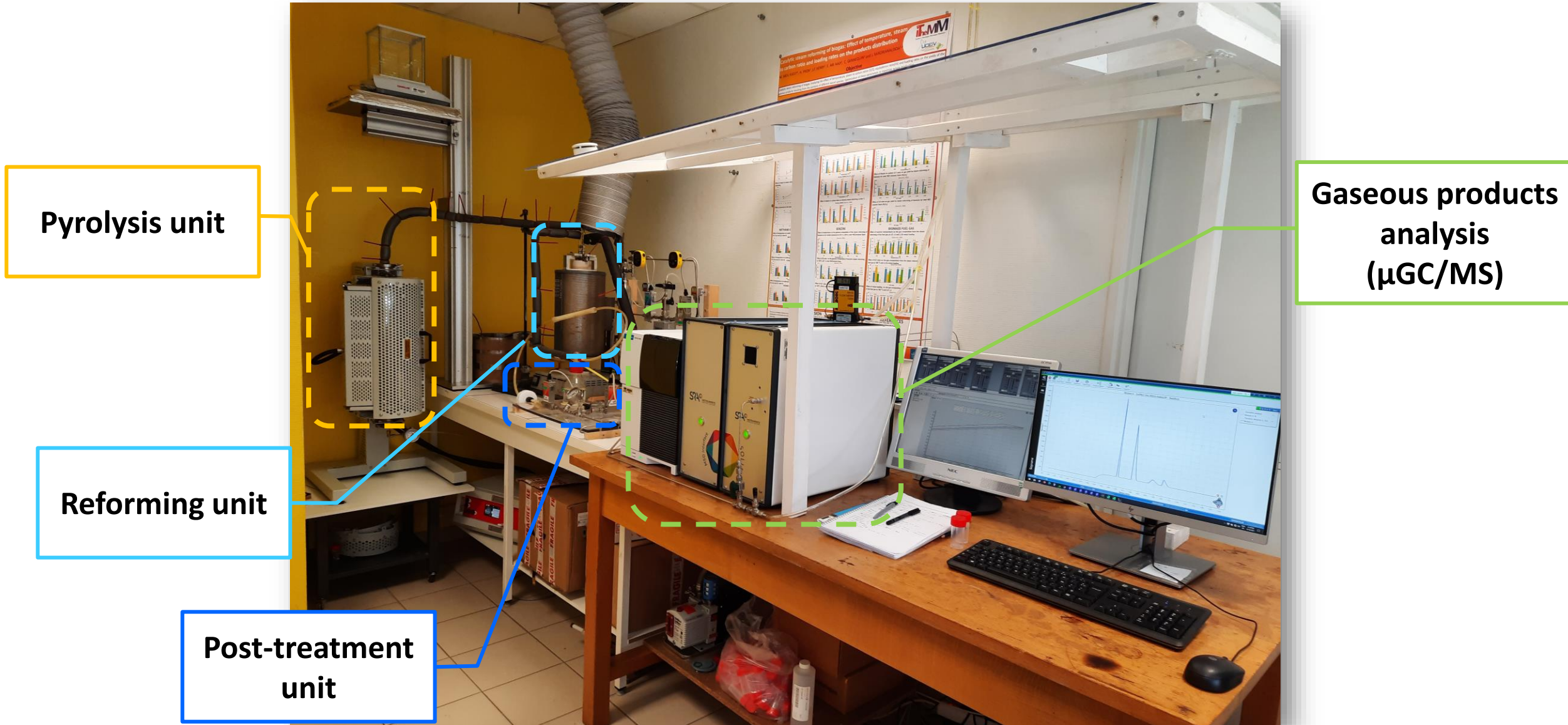


- Bio-oil:



Hybrid reforming:

CO₂ et H₂O vapor produced by the biomass pyrolysis → reactants for the reforming of the pyrolysis volatiles



Materials and Methods

Parameter ranges:

Pyrolysis unit:

- Biomass: up to **10g**
- Temperature: **300 – 800°C**
- Heating rate: **5 – 100°C/min**
- Volatiles residence time: **50 – 250 s**

Catalytic reforming unit:

- Gas and bio-oil volatiles
- Temperature: **600 – 800°C**
- GHSV: **900 - 25000 h⁻¹**
- Volatiles residence time: **10 – 120 s**

Carrier gas:

- Nature:
nitrogen, air or water vapor
- Flowrate:
25 – 300 mL/min

Catalyst:

- Type: **bulk or supported on alumina**
- Active phase:
Nickel, Cobalt, Cobalt-Nickel
- Metal loading: **0 – 30%**

Materials and Methods

Characterizations:

Biomass

- Elemental analysis
(C, H, O, N, S...)
- Chemical composition
(cellulose, hemicellulose,
lignin)
- Physical properties
(density, size, porosity)

Bio-oil

- Chemical composition:
BTEX,
phenols,
PAH (polycyclic aromatic
hydrocarbons),
others (furfural)

Catalyst

- TGA (Thermogravimetric
Analysis)
- DTA (Differential
Thermal Analysis)
- Porosimetry analysis,
BET surface area
- XRD (X-ray diffraction)
- SEM (Scanning Electron
Microscopy) images
- EDX (Energy-dispersive
X-ray spectroscopy)

Materials and Methods

Biomass



Oak wood chips

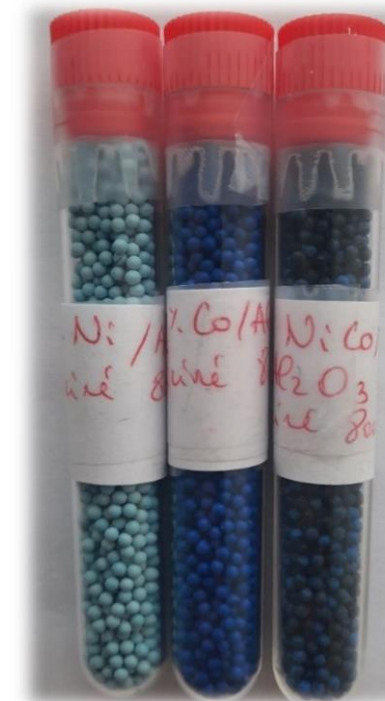


Flax shives

Catalysts



Bulk catalysts

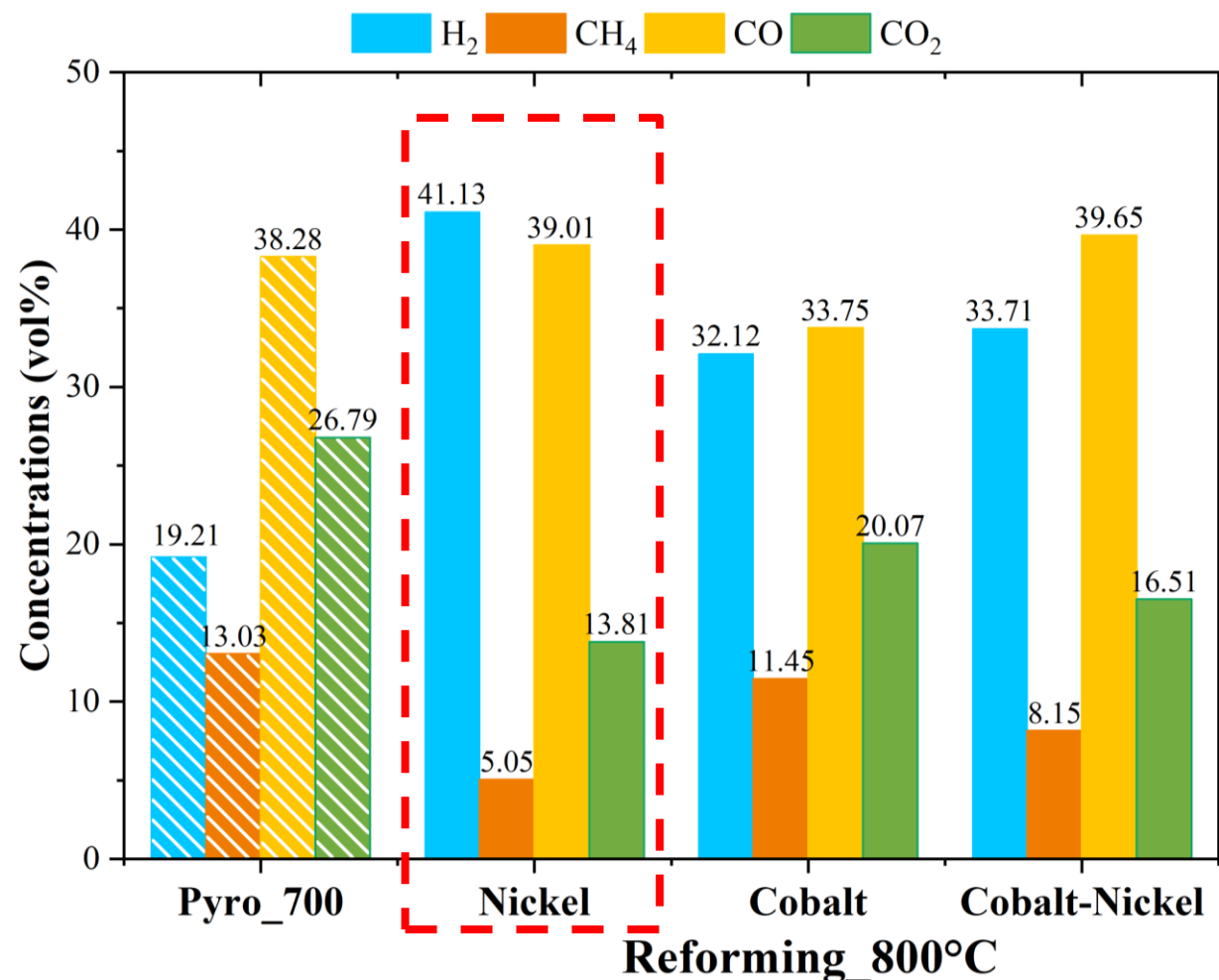
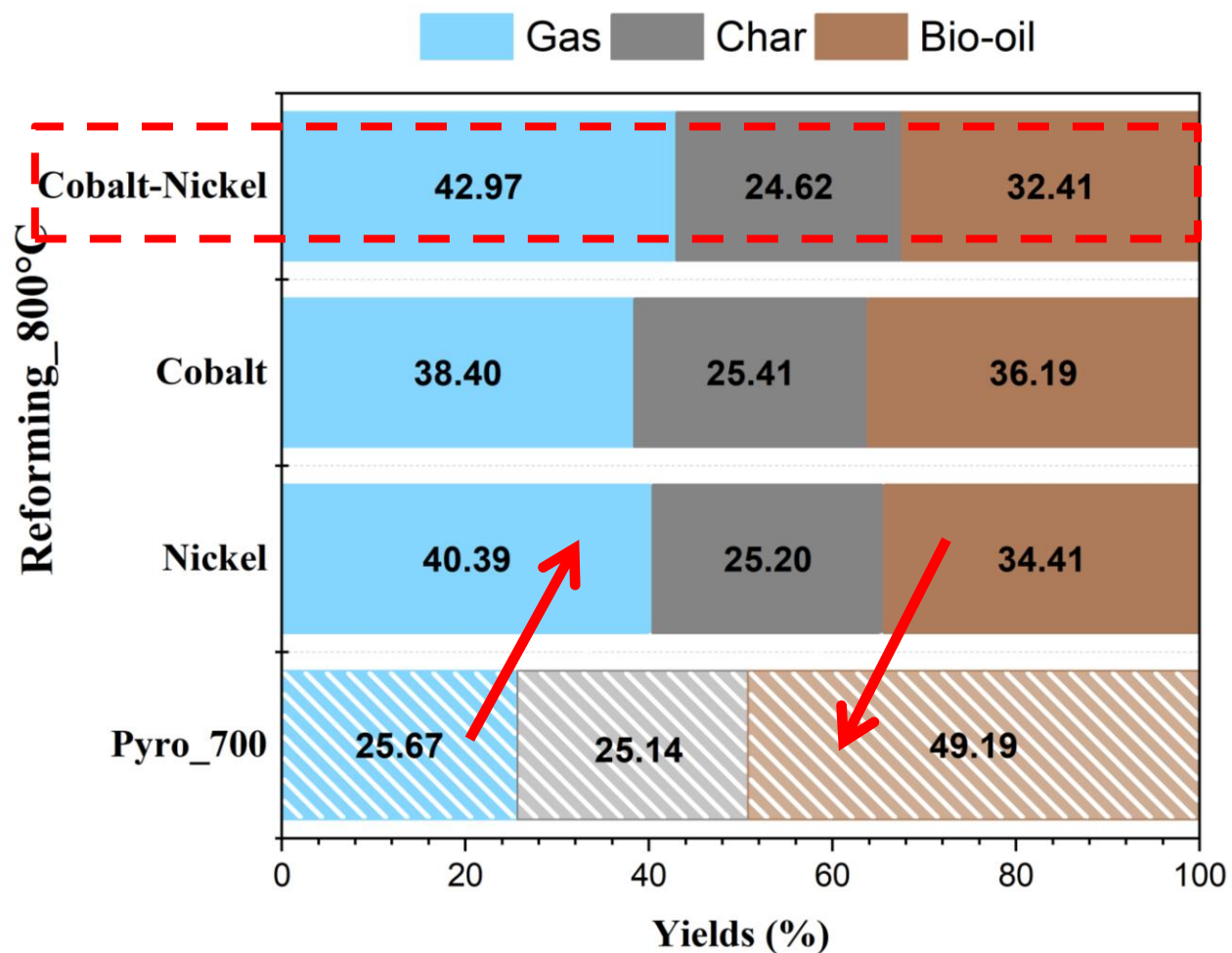


Supported catalysts

Cobalt, Nickel and Cobalt-Nickel

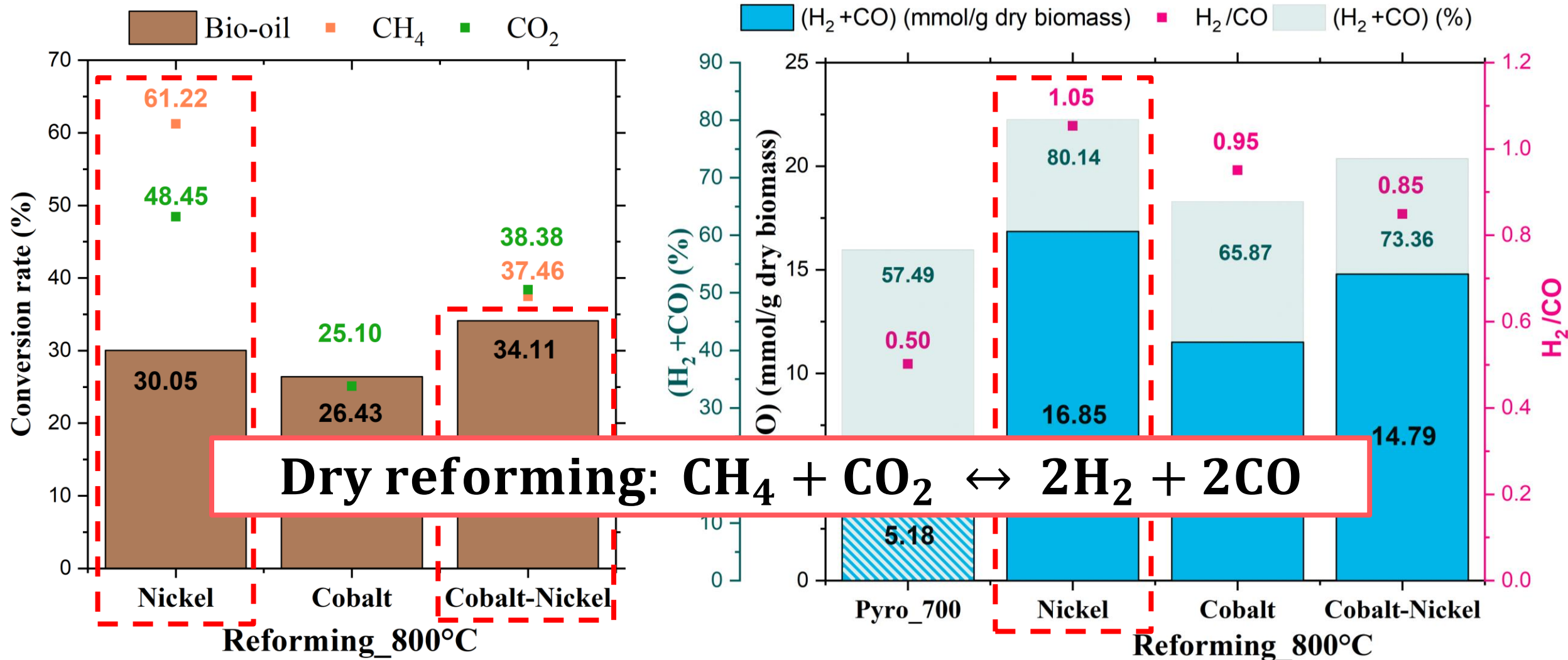
Results and discussions

1) Effect of the active phase of bulk catalysts with oak wood chips as biomass



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Materials and Methods

Biomass



Oak wood chips



Flax shives

Catalysts



Bulk catalysts

20%Ni/Al₂O₃

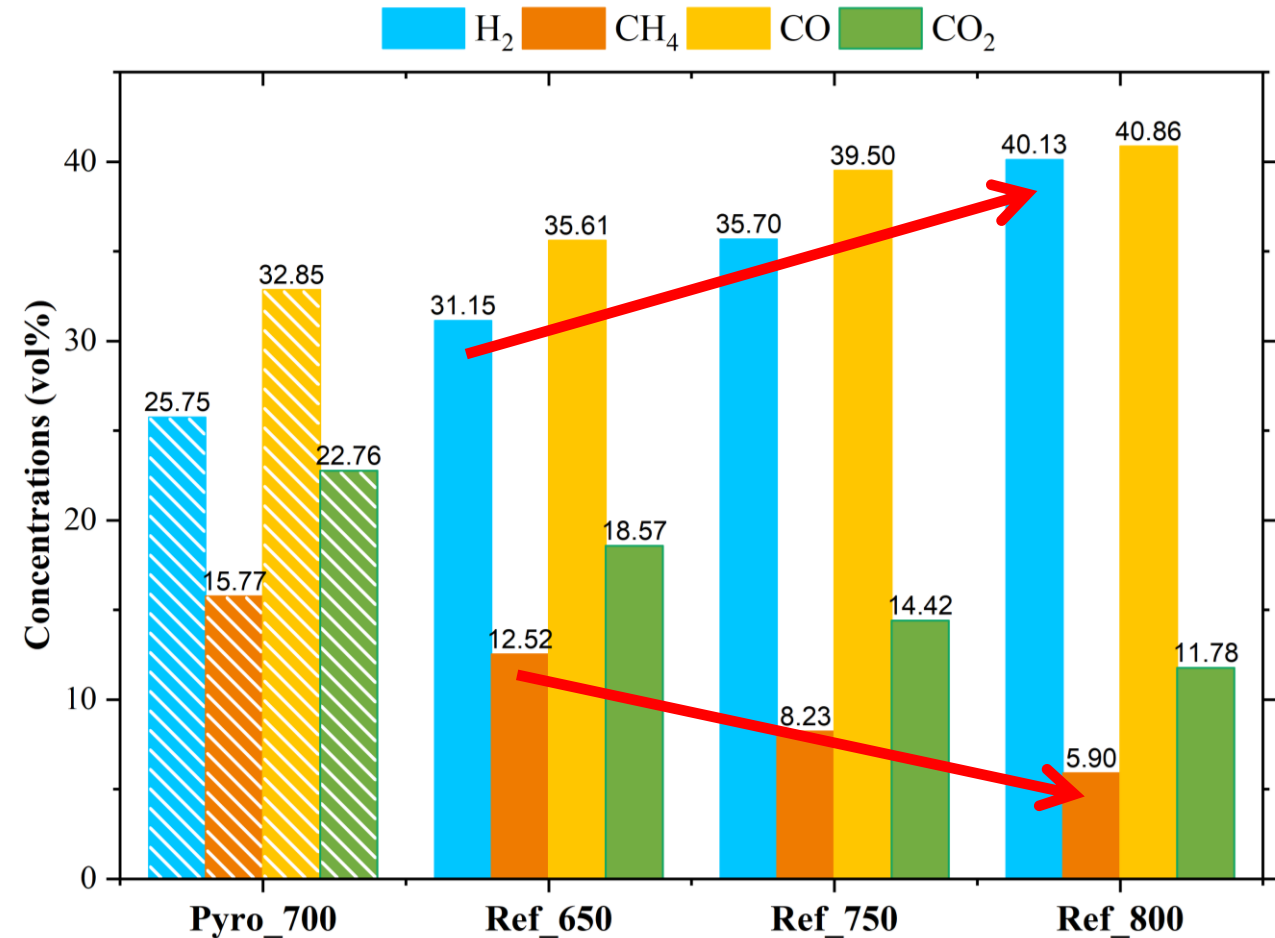
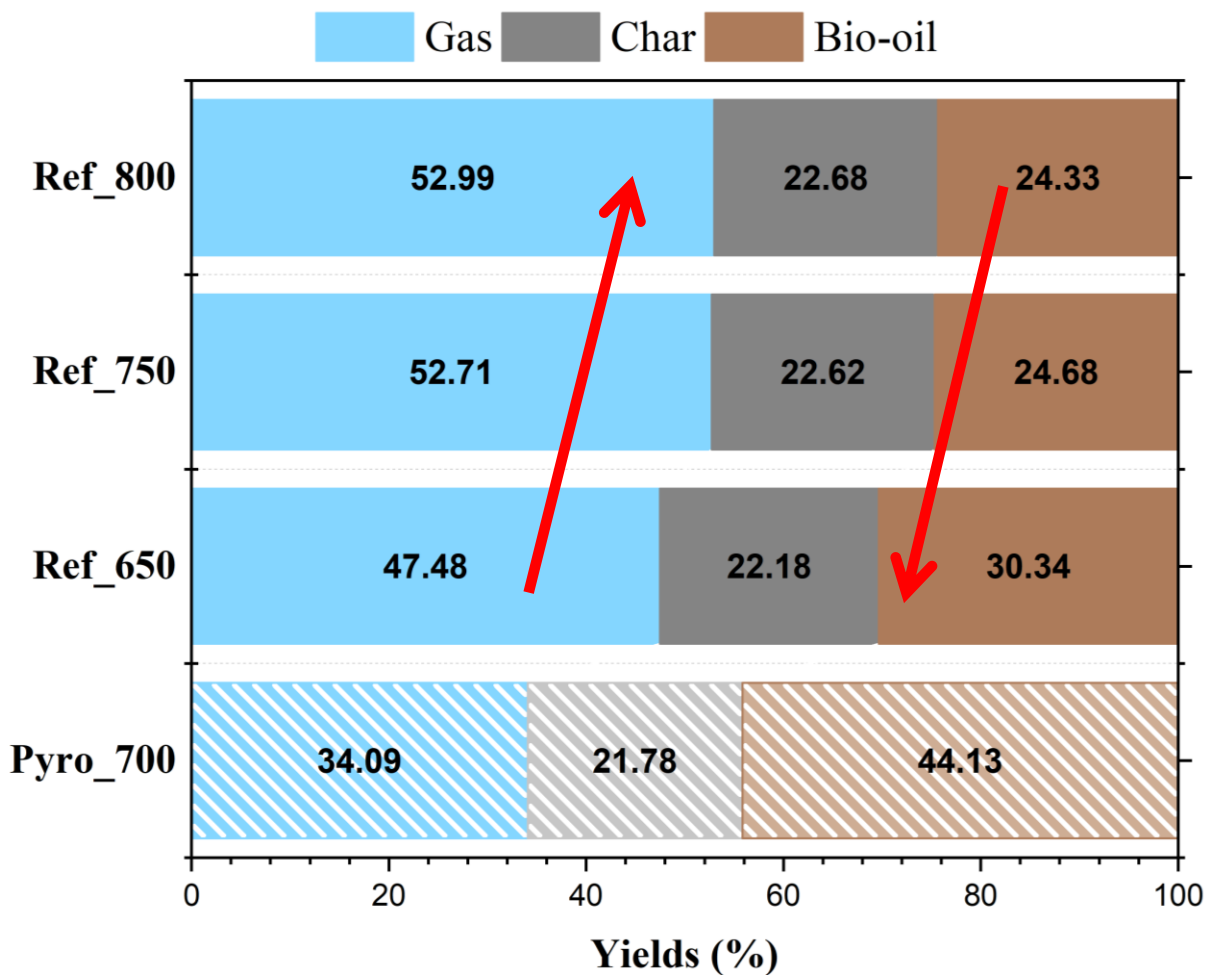


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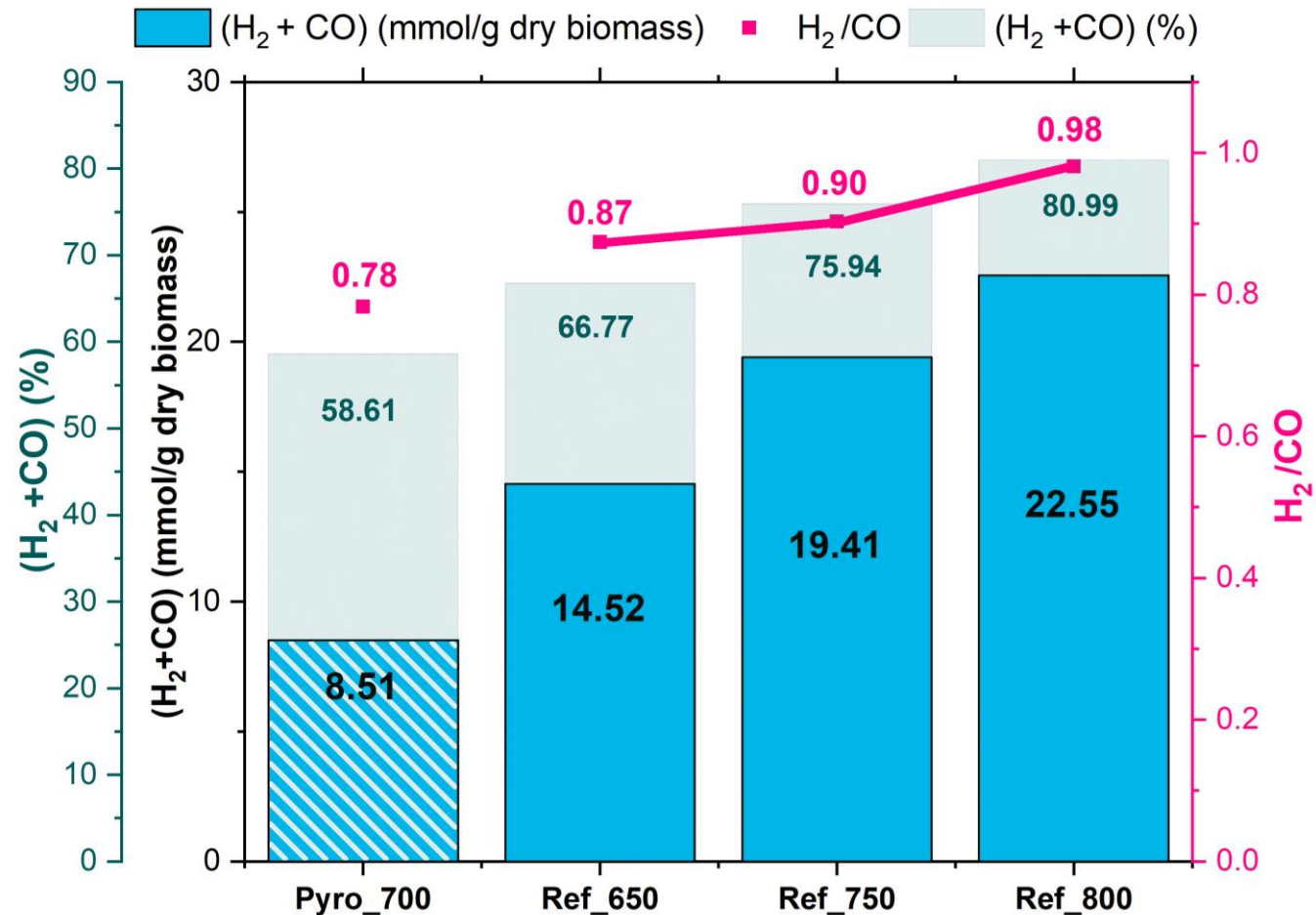
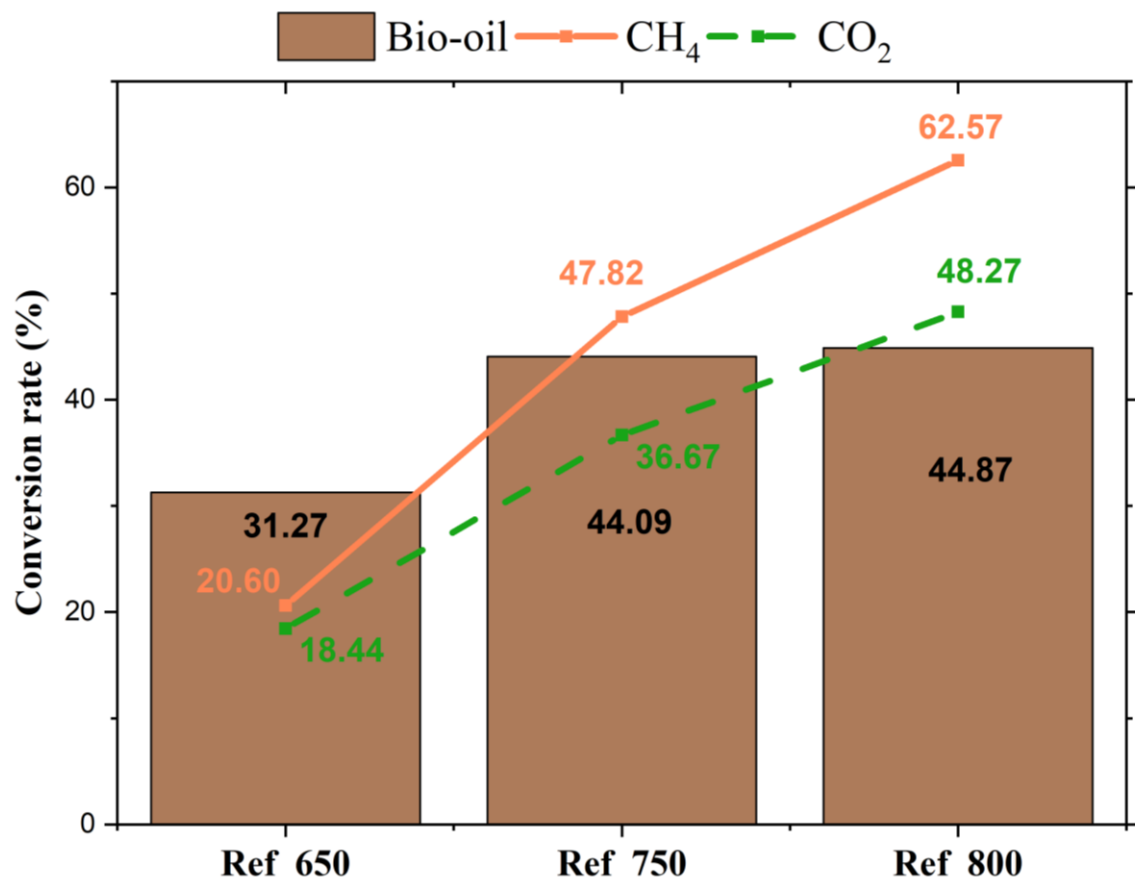
Results and discussions

2) Effect of reforming temperature (flax shives and 20%Ni/Al₂O₃)



Results and discussions

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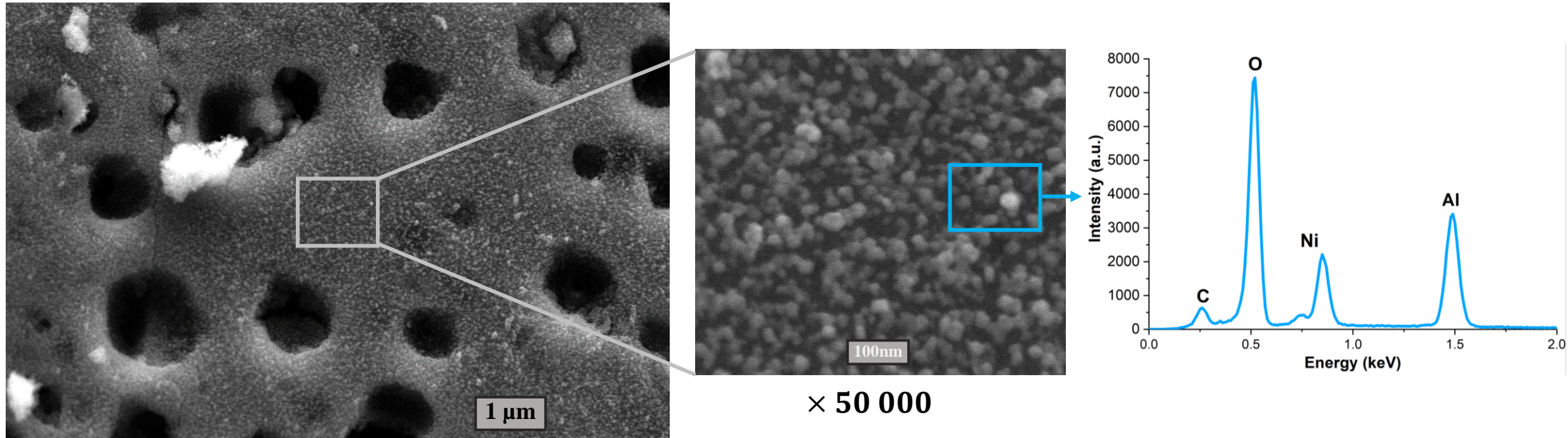


Reforming at 800°C favors the bio-oil conversion and improves the syngas production (H₂)

Results and discussions

Characterization of catalysts by SEM images and EDX analysis

Initial catalyst 20% Ni/Al₂O₃



× 10 000

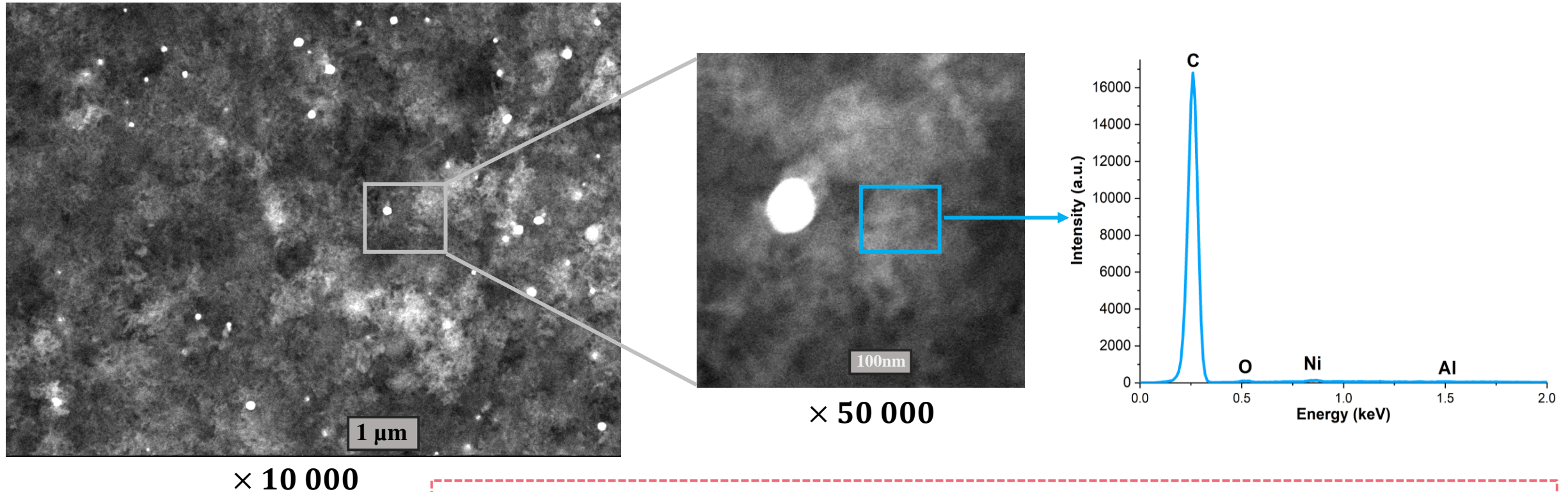
× 50 000

- Nickel particles (~30-40nm) → proven by the EDX analysis (Ni, Al, O et C)
- Pores (~7 nm) between the particles de Ni
- Large pores (1 μm) → initial pores present in the alumina beads non covered by Ni

Results and discussions

Characterization of catalysts by SEM images and EDX analysis

20% Ni/Al₂O₃ after reforming at 800°C



- Large Ni particles (~100 nm) → Agglomeration of the Ni → Sintering of the catalyst
- Presence of filamentous carbon (~50 nm) (confirmed by EDX) → carbon deposition → deactivation of active Ni sites

Materials and Methods

Dry reforming (CO₂) of methane:



$$\rightarrow \text{H}_2/\text{CO} = 1$$

Objective: intensify
steam reforming for
H₂ production



Steam reforming (H₂O) of methane:



$$\rightarrow \text{H}_2/\text{CO} = 3$$

Materials and Methods

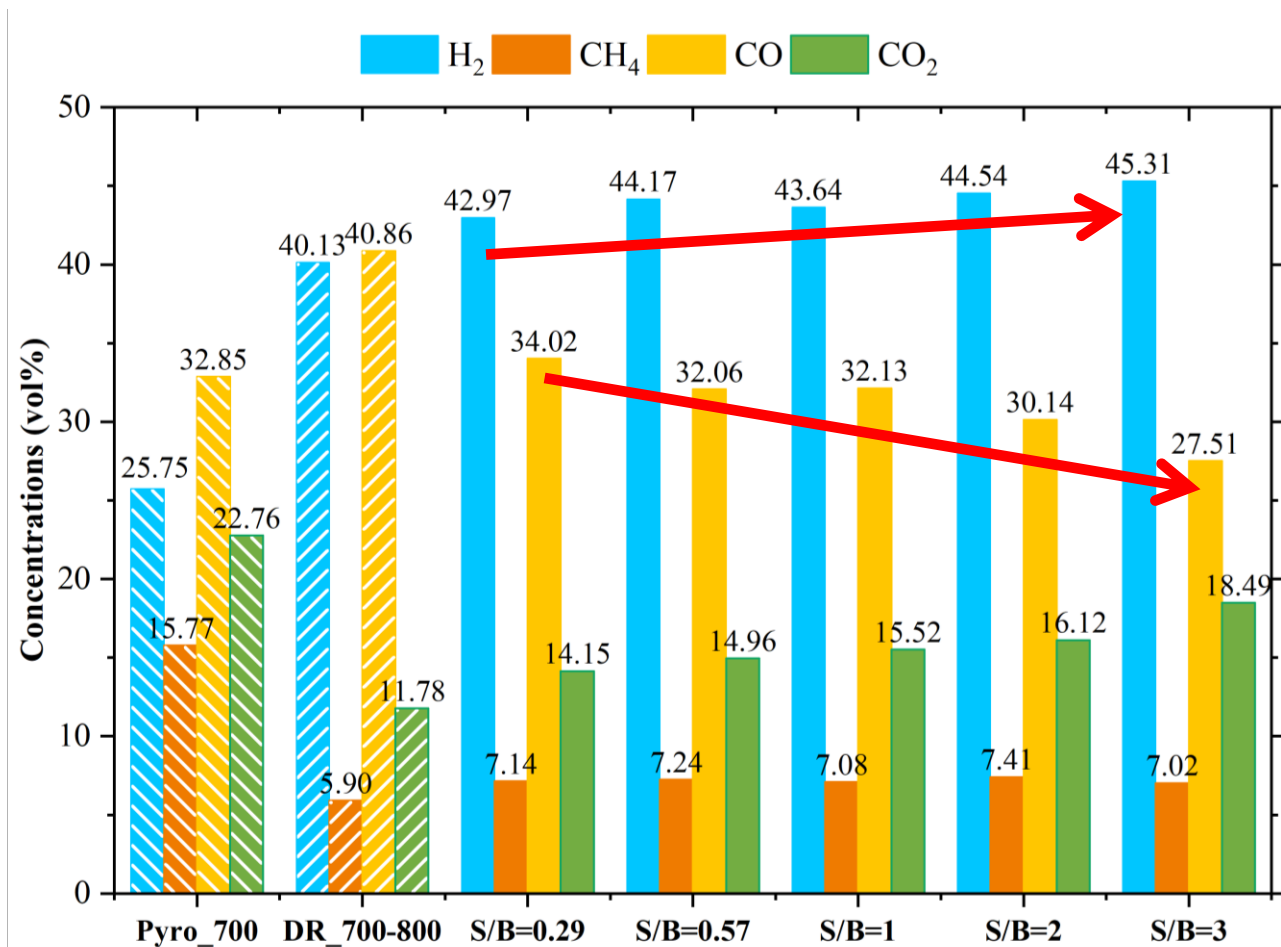
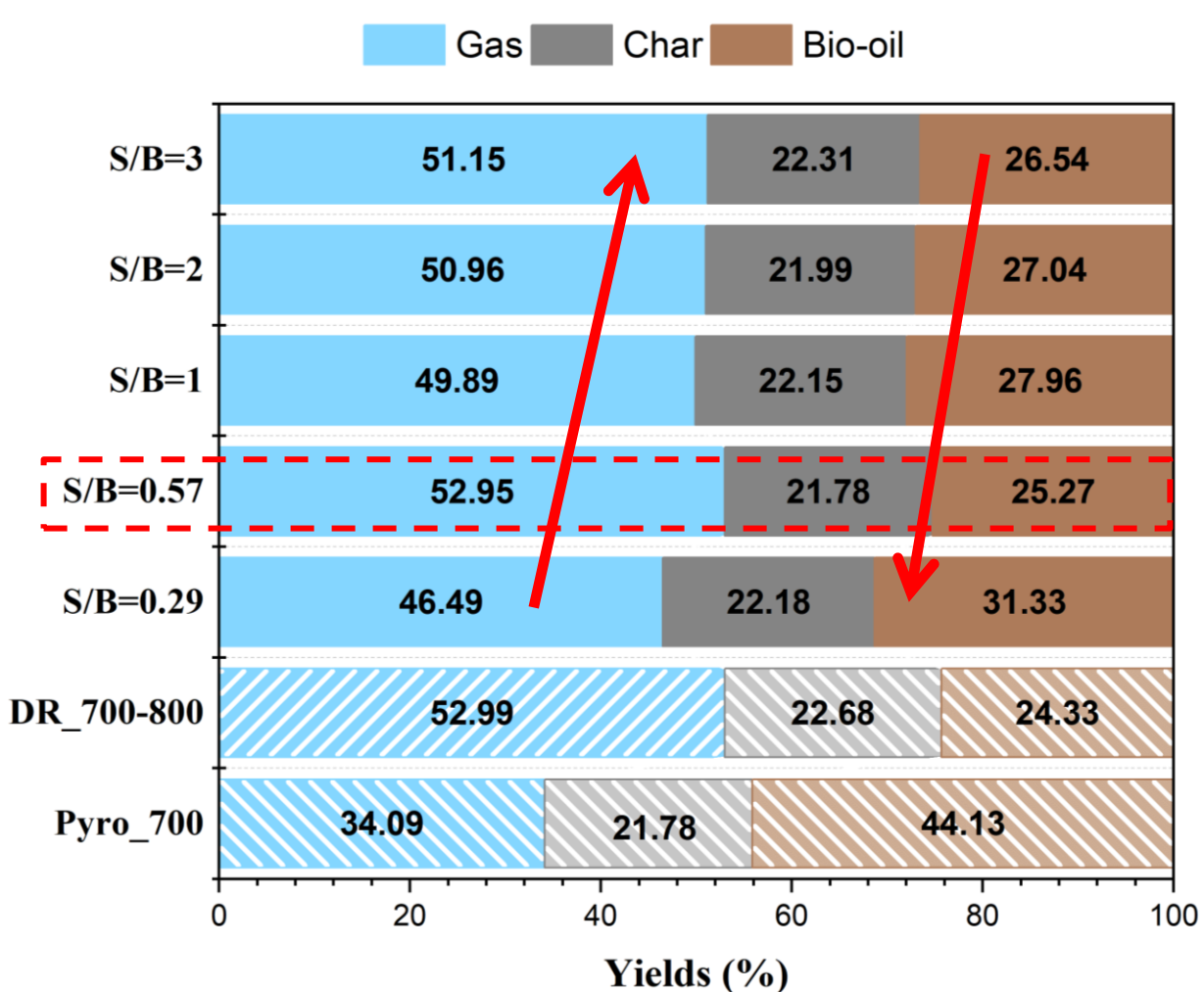
Steam to biomass ratio S/B

$$\text{Steam to biomass ratio: } S/B = \frac{\text{Water vapor flow rate}}{\text{biomass flow rate}}$$

Steam feed (g.h ⁻¹)	0.5	1	1.75	3.5	5.25
S/B ratio	0.29	0.57	1	2	3

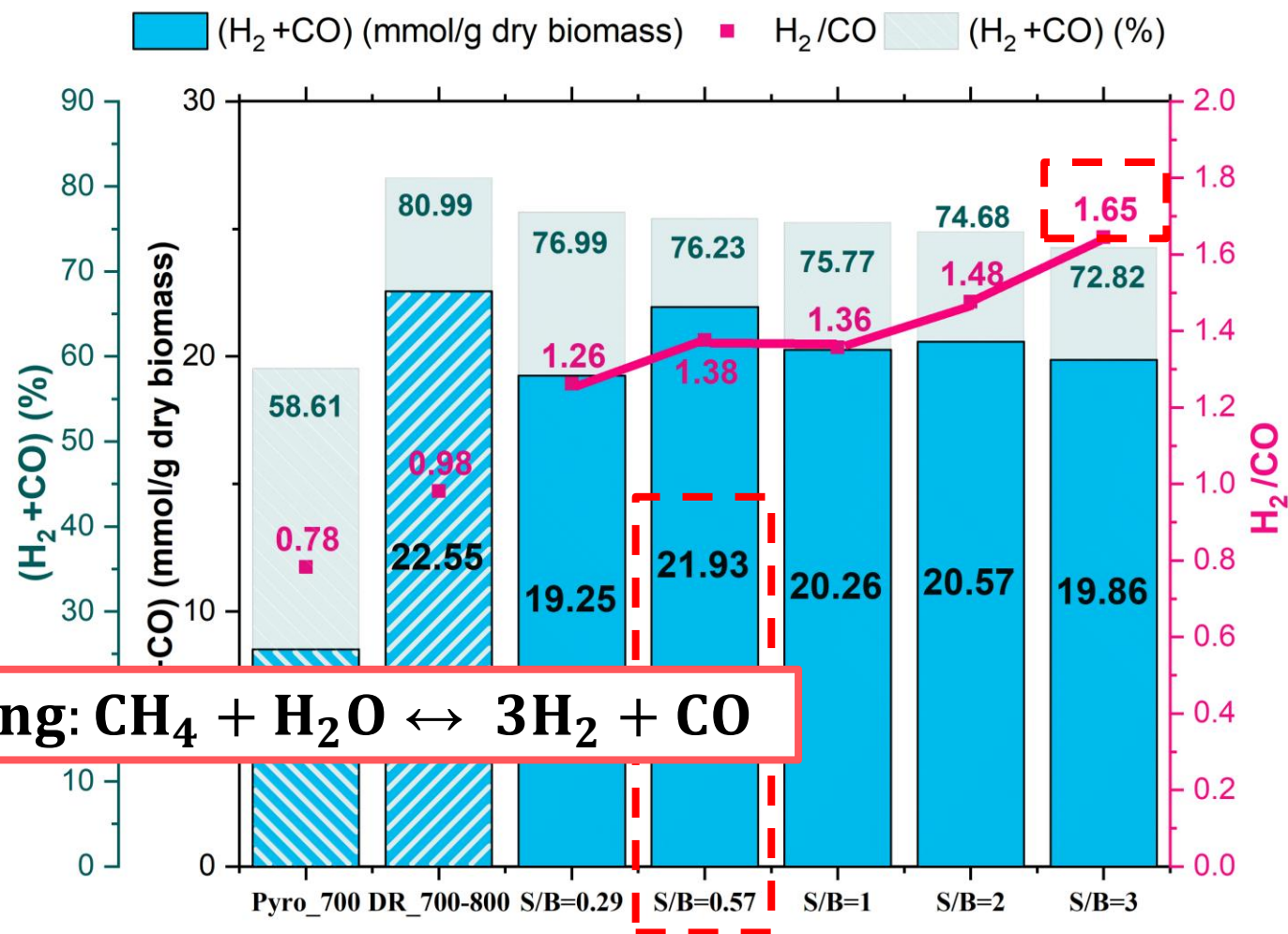
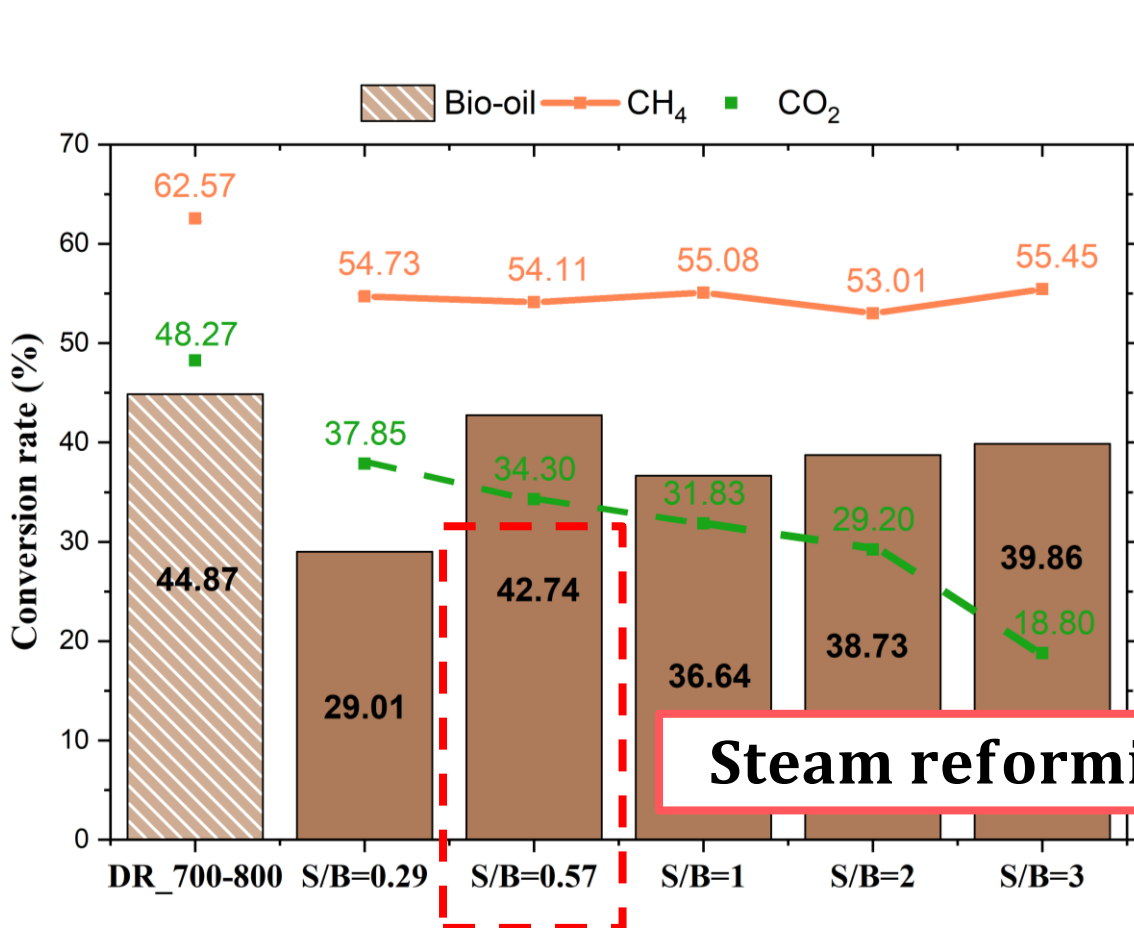
Results and discussions

3) Effect of S/B ratio on steam reforming ($T_{ref}=800^{\circ}\text{C}$, 20%Ni/Al₂O₃)



Results and discussions

3) Effect of S/B ratio on steam reforming ($T_{ref}=800^{\circ}\text{C}$, 20%Ni/Al₂O₃)



Conclusion

Pyrolysis/ reforming

- **Valorization of biomass** into high added value products such as syngas

Nickel

- Low cost, high availability, strong activity and stability
- Suffers from carbon deposition and sintering leading to its deactivation

Cobalt-Nickel

- Increases gas production and improves bio-oil conversion
- Reduces carbon deposition

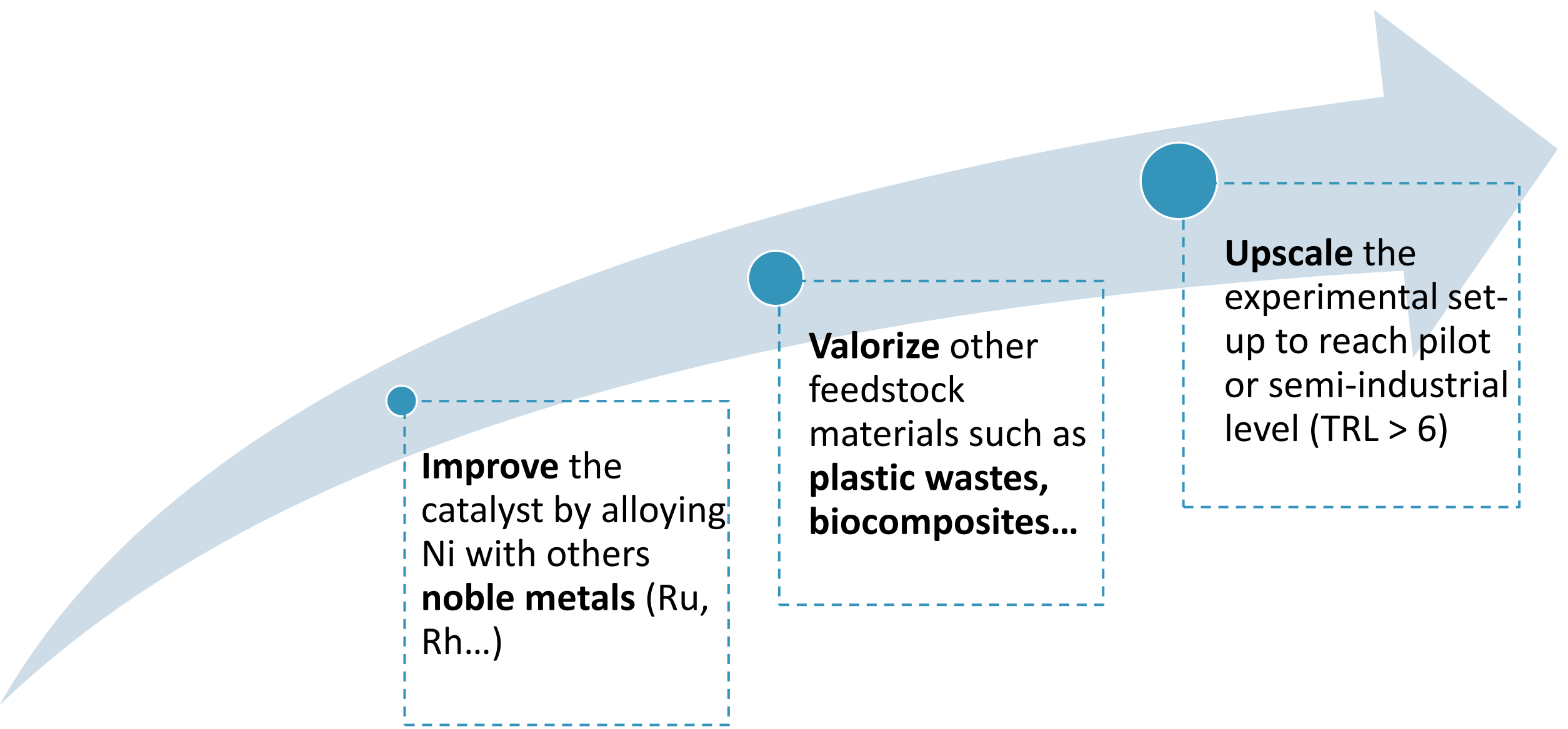
Temperature [650 – 800°C]

- Increasing the temperature **improves the syngas** production
- Optimal conditions: **800°C (reduces carbon deposition)**

Steam reforming S/B = [0.29-3]

- Adding water vapor poorly impacts the products distribution but strongly enhances H₂ production
- Optimal conditions: **S/B = 0.6 for max syngas; S/B = 3 for max H₂**

Perspectives



Improve the catalyst by alloying Ni with others **noble metals** (Ru, Rh...)

Valorize other feedstock materials such as **plastic wastes, biocomposites...**

Upscale the experimental set-up to reach pilot or semi-industrial level (TRL > 6)




Our recent publications on the topic

Environmental Chemistry Letters (2021) 19:2825–2872
<https://doi.org/10.1007/s10311-021-01190-2>

REVIEW



Pyrolysis-catalytic upgrading of bio-oil and pyrolysis-catalytic steam reforming of biogas: a review





Mira Abou Rjeily¹  · Cédric Gennequin²  · Hervé Pron¹ · Edmond Abi-Aad² · Jaona Harifidy Randrianalisoa¹ 

Waste and Biomass Valorization
<https://doi.org/10.1007/s12649-022-01848-0>

ORIGINAL PAPER



Detailed Analysis of Gas, Char and Bio-oil Products of Oak Wood Pyrolysis at Different Operating Conditions




Mira Abou Rjeily^{1,4}  · Fabrice Cazier²  · Cédric Gennequin^{3,4}  · Jaona Harifidy Randrianalisoa^{1,4} 

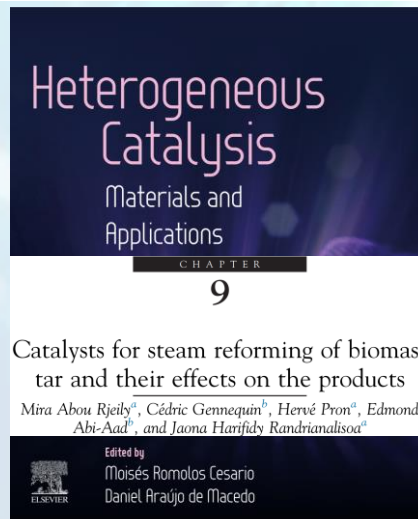
Waste and Biomass Valorization
<https://doi.org/10.1007/s12649-022-02012-4>

ORIGINAL PAPER



Biomass Pyrolysis Followed by Catalytic Hybrid Reforming for Syngas Production

Mira Abou Rjeily^{1,3}  · Muriel Chaghouri^{2,3} · Cedric Gennequin^{2,3}  · Edmond Abi Aad^{2,3} · Herve Pron^{1,3} · Jaona Harifidy Randrianalisoa^{1,3} 





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Thank you for your attention



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